

## Original Research

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# Synergistic conversion of spent mobile phone batteries and industrial lignin into the $\text{NiCo}_2\text{S}_4/\text{Co}_9\text{S}_8@\text{LC}$ composite with enhanced sodium storage performance

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## Abstract

This study systematically investigated the  $\text{NiCo}_2\text{S}_4/\text{Co}_9\text{S}_8@\text{LC}$  composite synthesized from spent mobile phone batteries and industrial lignin, focusing on its sodium storage characteristics. A hydrothermal method was employed to successfully fabricate  $\text{NCS/CS@LC}_{50}$ , exhibiting a honeycomb-like morphology through the precise control of lignin content. This composite integrated the high electrochemical activity of  $\text{NiCo}_2\text{S}_4$  and  $\text{Co}_9\text{S}_8$  with the superior conductivity of carbon materials, demonstrating promising sodium storage performance. The results indicated that  $\text{NCS/CS@LC}_{50}$  exhibited a high specific discharge capacity, i.e., an initial discharge specific capacity of  $1,062.8 \text{ mAh g}^{-1}$ , and outstanding cycling stability. The unique architecture of  $\text{NCS/CS@LC}_{50}$  facilitated the effective insertion and extraction of  $\text{Na}^+$ , allowing the material to preserve its structural stability throughout repeated charge-discharge processes, which in turn greatly improved the battery's cycling performance. At elevated current densities, such as  $2.0 \text{ A g}^{-1}$ ,  $\text{NCS/CS@LC}_{50}$  continued to exhibit a high specific discharge capacity ( $208.7 \text{ mAh g}^{-1}$ ), demonstrating excellent rate performance. This research introduces an innovative approach to effectively recycle and reuse spent mobile phone batteries and industrial lignin, while also providing new insights into the design of electrode materials for sodium-ion batteries.

**Keywords:** Spent batteries, Industrial lignin,  $\text{NiCo}_2\text{S}_4/\text{Co}_9\text{S}_8@\text{LC}$ , Biochar, Sodium storage

## Highlights

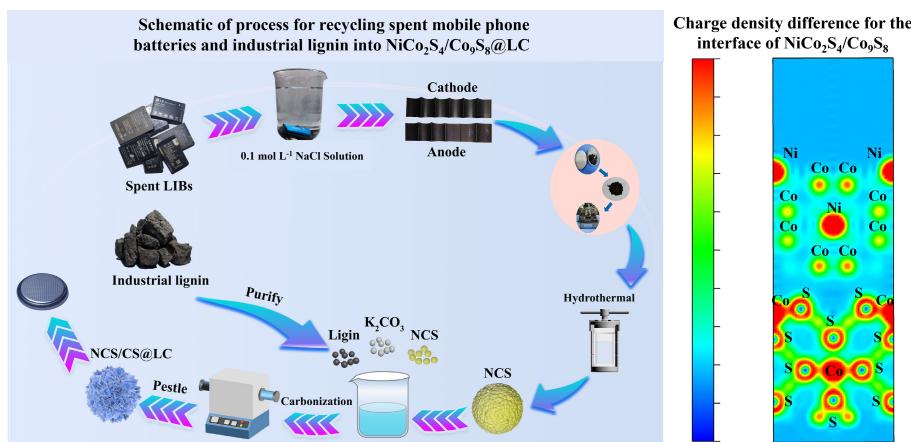
- This study offers a novel strategy for the recycling of industrial lignin and spent LIBs.
- This approach significantly reduces the synthesis cost of anode materials.
- The co-recycled product  $\text{NCS/CS@LC}_{50}$  demonstrates superior sodium storage performance.
- $\text{Co}_9\text{S}_8$  and lignin-derived carbon exert a pronounced enhancing effect on the sodium storage.

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## Graphical abstract



## Introduction

With advancements in science and technology, alongside improvements in living standards, mobile phones have become essential components of daily life. However, mobile phone batteries typically have a limited lifespan and generally necessitate replacement within a few years<sup>[1]</sup>. Moreover, as mobile phone technology continues to evolve, the frequency with which consumers upgrade their devices is also increasing, leading to a substantial accumulation of spent mobile phone batteries. Improper disposal of these batteries poses significant risks to the environment and human health, and also results in a considerable waste of metal resources<sup>[2]</sup>.

Lignin is a complex natural polymer primarily composed of phenylpropane structural units, representing approximately 30% of the Earth's non-fossil organic carbon. It constitutes a significant by-product in both the papermaking industry and biorefinery processes, with an annual production volume ranging from 50–70 million tons<sup>[3]</sup>. Despite its abundance, less than 5% of lignin is currently valorized for the production of high-value commercial products such as adhesives, dispersants, and surfactants<sup>[4]</sup>. Alarming, over 90% of industrial lignin is either discarded as waste or incinerated as low-value fuel, leading to substantial resource wastage and environmental pollution<sup>[5]</sup>.

Therefore, it is crucial to recycle spent mobile phone batteries and industrial lignin to not only mitigate pollution risks to the environment but also to reduce the demand for new resources, thereby promoting resource recycling and supporting sustainable development. If the synergistic resource recovery of these two types of solid wastes can be realized, their respective advantages can be fully leveraged, thereby achieving optimal resource allocation and maximizing resource utilization efficiency.

Sodium-ion batteries (SIBs) possess the potential to supplant lithium-ion batteries (LIBs) because of considerable advantages regarding resource abundance, safety, low temperature performance, rapid charging capabilities, and environmental friendliness<sup>[6]</sup>. As is well known, the anode material serves as a pivotal component in SIBs, with its performance exerting a direct influence on the overall efficacy of these energy storage systems<sup>[7]</sup>. Transition metal sulfides that operate via the transformation reaction mechanism have garnered significant research interest owing to their high theoretical specific capacity, excellent ionic transport properties, and superior mechanical and thermal stability. Notably, bimetallic sulfides demonstrate enhanced electrochemical performance relative to their single-metal counterparts, which can be

credited to the synergistic effects arising from the interaction of dissimilar metal ions. Among the reported bimetallic sulfides, NiCo<sub>2</sub>S<sub>4</sub> has been deliberately engineered and synthesized to serve as a potential anode material for SIBs. Nevertheless, pure NiCo<sub>2</sub>S<sub>4</sub> presents certain limitations concerning cycle stability, volumetric changes, first-cycle Coulombic efficiency, kinetic performance, and cost-effectiveness<sup>[8]</sup>. Consequently, it is imperative to modify NiCo<sub>2</sub>S<sub>4</sub> to enhance its sodium storage capabilities. And researchers often adopt a composite material design strategy that synergistically integrates NiCo<sub>2</sub>S<sub>4</sub> with various carbon materials to bolster both structural integrity and electrochemical performance. For instance, Xi et al. prepared hollow mesoporous carbon spheres encapsulating NiCo<sub>2</sub>S<sub>4</sub> nanoparticles, demonstrating superior rate performance and achieving a high capacity of 271 mAh g<sup>-1</sup> at 10 A g<sup>-1</sup><sup>[9]</sup>. However, the carbon sources are predominantly conventional industrial products, which do not fully align with the principle of 'treating waste with waste' in the context of deep resource recycling. To date, no studies have been reported on enhancing NiCo<sub>2</sub>S<sub>4</sub>'s sodium storage performance through the combination of industrial lignin-derived carbon and NiCo<sub>2</sub>S<sub>4</sub>.

In this study, NiCo<sub>2</sub>S<sub>4</sub> was synthesized from spent mobile phone batteries via a hydrothermal method, an approach characterized by straightforward operation, high product purity, controllable reaction parameters, and environmental sustainability<sup>[10]</sup>. The synthesized NiCo<sub>2</sub>S<sub>4</sub> was carbonized in conjunction with lignin, resulting in the successful preparation of NiCo<sub>2</sub>S<sub>4</sub>/Co<sub>9</sub>S<sub>8</sub>@LC. This process enables the synergistic high-value utilization of both types of waste. Moreover, a series of characterizations was conducted to investigate the effect of Co<sub>9</sub>S<sub>8</sub> and lignin-derived carbon on the structure, morphology, and sodium storage properties of NiCo<sub>2</sub>S<sub>4</sub>. This approach not only substantially lowers the synthesis cost of anode materials but also promotes the sustainable utilization of resources and environmental protection. Importantly, it offers a novel strategy for the recycling and reutilization of industrial lignin and spent LIBs.

## Experiments

### Synthesis of materials

#### Synthesis of NiCo<sub>2</sub>S<sub>4</sub>

The processes of discharging, disassembling, and dissolving spent mobile phone batteries (Nokia), along with the hydrothermal synthesis of NiCo<sub>2</sub>S<sub>4</sub>, have been detailed in a previous study<sup>[11]</sup>.

### Purification of industrial lignin

Two hundred g of industrial lignin (Jilin Papermaking (Group) Co., Ltd) was weighed and dissolved in NaOH solution with a pH  $\geq 12$  under continuous stirring for 2 h. Once the lignin was fully dissolved, the solution was filtered to remove insoluble impurities, and the filtrate was collected. Subsequently, while continuously stirring, 50% (w/w) sulfuric acid was slowly added to the filtrate to adjust the pH of the solution to 2. The mixture was stirred for an additional 2 h to allow lignin precipitation. The solution was then allowed to stand for 24 h, after which the precipitated lignin was collected by filtration. The collected lignin was washed thoroughly and subjected to freeze-drying to obtain purified lignin.

### Synthesis of $\text{NiCo}_2\text{S}_4/\text{Co}_9\text{S}_8@\text{LC}$

A total of 0.2 g of  $\text{NiCo}_2\text{S}_4$  was introduced into an ethanol-water mixture ( $V_{\text{ethanol}} : V_{\text{water}} = 1:4$ ). The dispersion was subjected to multiple cycles of ultrasonic treatment to ensure homogeneity. Subsequently, lignin was introduced into a separate ethanol-water solution ( $V_{\text{ethanol}} : V_{\text{water}} = 1:4$ , C = 2 mg/mL) under ultrasonic conditions for thorough dispersion. The weight ratios of lignin to  $\text{NiCo}_2\text{S}_4$  were set at 25%, 50%, and 75%. The two dispersions were then combined, and the pH of the final solution was regulated to 12 by incorporating a 20% (w/w) NaOH solution. The mixture was subjected to magnetic stirring at ambient temperature for a duration of 30 min, and then subjected to ultrasonic processing for another 30 min. This procedure was carried out repeatedly until a uniformly dispersed solution was obtained. Thereafter, the pH was lowered to 2 by adding a 50% (w/w) sulfuric acid solution. The solution was left undisturbed for 12 h to enable the full precipitation of  $\text{NiCo}_2\text{S}_4$  and lignin. Finally, the  $\text{NiCo}_2\text{S}_4$ -lignin composite was collected via centrifugation and dried.

The above-mentioned synthesized  $\text{NiCo}_2\text{S}_4$ -lignin composites were dispersed in 50 mL of deionized water, and then  $\text{K}_2\text{CO}_3$  was added as an activator at a  $\text{K}_2\text{CO}_3$ -to-lignin weight ratio of 1:1. The resulting mixture was continuously stirred for 4 h, subsequently dried at 80 °C, and finally ground into a fine powder for collection. Next, the sample was heated under a nitrogen atmosphere from ambient temperature to 250 °C at a heating rate of 10 °C/min and held at this temperature for 30 min. Subsequently, the temperature was further increased to 600 °C at the identical heating rate of 10 °C/min and maintained for 2 h to achieve complete carbonization of the lignin component. Afterward, the resulting product was thoroughly rinsed multiple times with deionized water and then dried at 100 °C to yield the final  $\text{NiCo}_2\text{S}_4/\text{Co}_9\text{S}_8@\text{LC}$  composite, which was designated as NCS/CS@LC<sub>25</sub>, NCS/CS@LC<sub>50</sub>, and NCS/CS@LC<sub>75</sub>, respectively.

### Characterization of materials, electrochemical measurements, and computational details

The structural and morphological characterization techniques, the electrochemical performance evaluation procedures, and the theoretical calculation details for the synthesized samples were included in the [Supplementary Material](#).

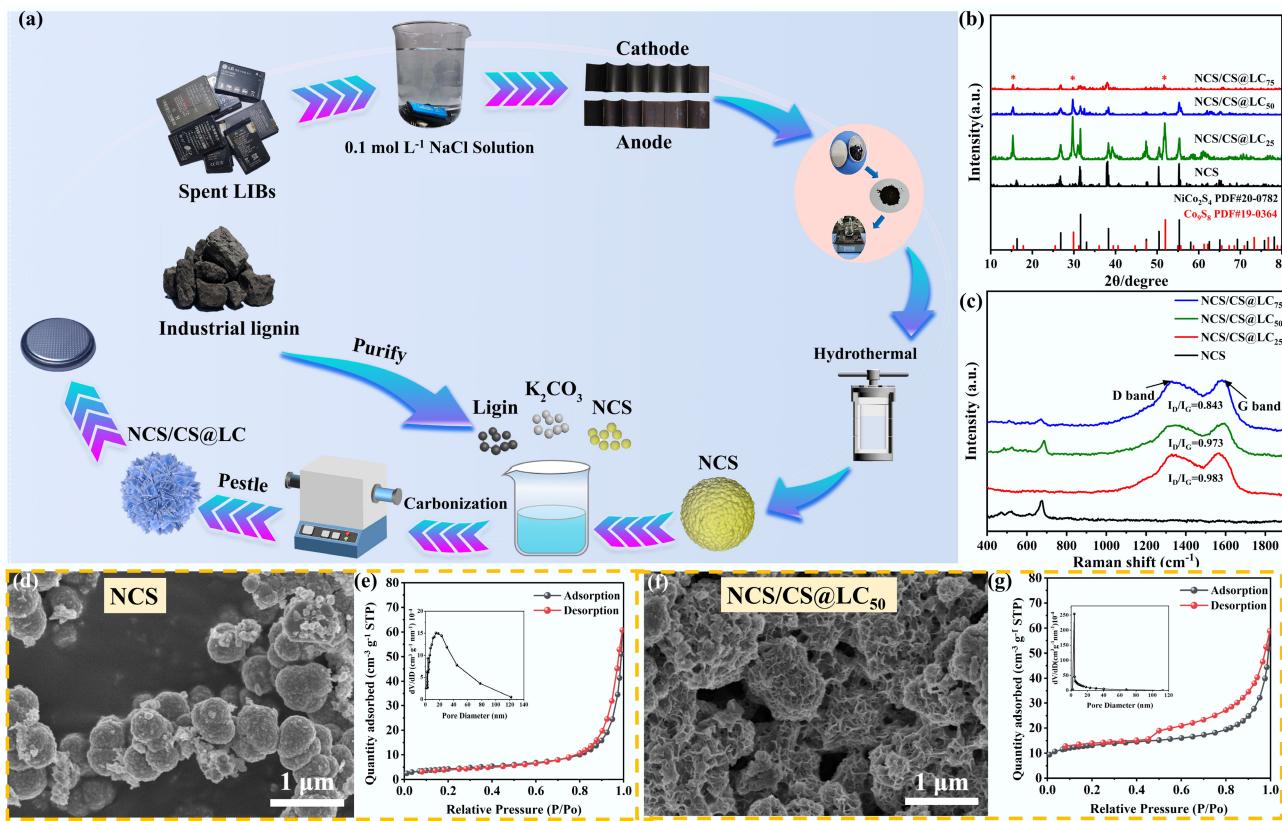
## Results and discussion

The flowchart illustrating the co-conversion process of spent mobile phone batteries and industrial lignin for the preparation of NCS/CS@LC is presented in [Fig. 1a](#). The XRD patterns of the synthesized samples are presented in [Fig. 1b](#). The observed diffraction peaks exhibited sharpness and high intensity, indicating a relatively complete crystal structure and elevated crystallinity. It was evident that the diffraction peaks of NCS aligned well with the standard card for  $\text{NiCo}_2\text{S}_4$  (JCPDS

No. 20-0782), confirming the successful synthesis of  $\text{NiCo}_2\text{S}_4$ . Upon incorporating varying amounts of lignin into NCS and subsequently carbonizing the composites in a nitrogen atmosphere, a new phase of  $\text{Co}_9\text{S}_8$  (JCPDS No.19-0364) emerged, indicated by '\*' in [Fig. 1b](#). Notably, it appeared that  $\text{NiCo}_2\text{S}_4$  may partially convert into  $\text{Co}_9\text{S}_8$  due to the reorganization or recombination of metal ions from  $\text{NiCo}_2\text{S}_4$  with sulfur ions present in the reaction system under conditions of elevated temperature and pressure, resulting in novel metal sulfide phase formation<sup>[12]</sup>. In addition, the sulfur-containing functional groups in lignin, such as methylthio groups, release  $\text{S}^{2-}$  or  $\text{H}_2\text{S}$  during thermal decomposition, thereby sustaining a sulfidation atmosphere. Concurrently, the decomposition produces reductive gases such as CO and  $\text{H}_2$ , which lower the oxygen potential of the system and promote the generation of  $\text{Co}_9\text{S}_8$ . Ultimately, carbon materials derived from lignin may encapsulate these metal sulfides' surface to create a composite structure represented as NCS/CS@LC. The presence of other phases, such as  $\text{NiCo}_2\text{S}_4$  and  $\text{Co}_9\text{S}_8$ , leads to notably weak and nearly undetectable diffraction peaks for carbon within the synthesized materials. This suggested that the carbon produced post-carbonization was amorphous in nature<sup>[13]</sup>. Nevertheless, the Raman spectrum corroborated the existence of carbon within NCS/CS@LC, as depicted in [Fig. 1c](#).

Raman spectroscopy is a spectral analysis technique predicated on the Raman scattering effect, which elucidates molecular vibrational and rotational information of matter by examining the frequency difference between scattered and incident light. The G peak constitutes one of the most prominent characteristic peaks in carbon materials, primarily resulting from the stretching vibrations of  $\text{sp}^2$ -hybridized carbon atoms<sup>[14]</sup>. Conversely, the D peak signifies another critical characteristic peak in carbon materials, predominantly arising from defects or disordered structures within the carbon atomic lattice<sup>[15]</sup>. As illustrated in [Fig. 1c](#), it was evident that the typical D and G characteristic peaks were absent in NCS not co-carbonized with lignin; however, other samples exhibited significant D and G peaks located near 1,340 and 1,585  $\text{cm}^{-1}$ , respectively. These observations substantiated the presence of carbon within NCS/CS@LC. Furthermore, the intensity ratio of D and G peak ( $I_{\text{D}}/I_{\text{G}}$ ) is frequently utilized as an essential parameter for characterizing defect density in carbon materials<sup>[16]</sup>. A progressive decrease in  $I_{\text{D}}/I_{\text{G}}$  from 0.983 to 0.843 was noted, suggesting a reduction in amorphous or defective carbon content alongside an enhancement in graphitization degree. However, an excessively high degree of graphitization may not be advantageous, as it leads to an increase in ordered graphite layers while reducing interlayer spacing, concurrently diminishing surface defects. This results in fewer  $\text{Na}^+$  adsorption sites, which could consequently impair the sodium storage capacity<sup>[17]</sup>. High levels of graphitization may yield a densely compacted carbon material detrimental to  $\text{Na}^+$  diffusion and storage capabilities, thereby adversely affecting cycling performance and Coulombic efficiency, as well as limiting  $\text{Na}^+$  diffusion rates that negatively impact rate performance<sup>[18]</sup>. Therefore, achieving an optimal  $I_{\text{D}}/I_{\text{G}}$  value is crucial for attaining superior electrochemical performance, which will be further substantiated through subsequent analyses.

[Figure 1e, g](#), respectively, present the adsorption-desorption isotherms of NCS and NCS/CS@LC<sub>50</sub>, with the corresponding isotherms for the remaining samples provided in [Supplementary Fig. S1](#), which were used to determine the specific surface area and pore size distribution. All four isotherms displayed typical type-IV characteristics, evident from the hysteresis loop observed in the high-pressure region, where the desorption curve lagged behind the adsorption curve during the desorption process. This



**Fig. 1** (a) Schematic of the process for recycling spent mobile phone batteries and industrial lignin into NiCo<sub>2</sub>S<sub>4</sub>/Co<sub>9</sub>S<sub>8</sub>@LC. (b) XRD patterns of synthesized samples. (c) Raman spectral analysis of synthesized samples. (d) SEM images of NCS. (e) Adsorption-desorption isotherm of NCS. (f) SEM images of NCS/CS@LC<sub>50</sub>. (g) Adsorption-desorption isotherm of NCS/CS@LC<sub>50</sub>.

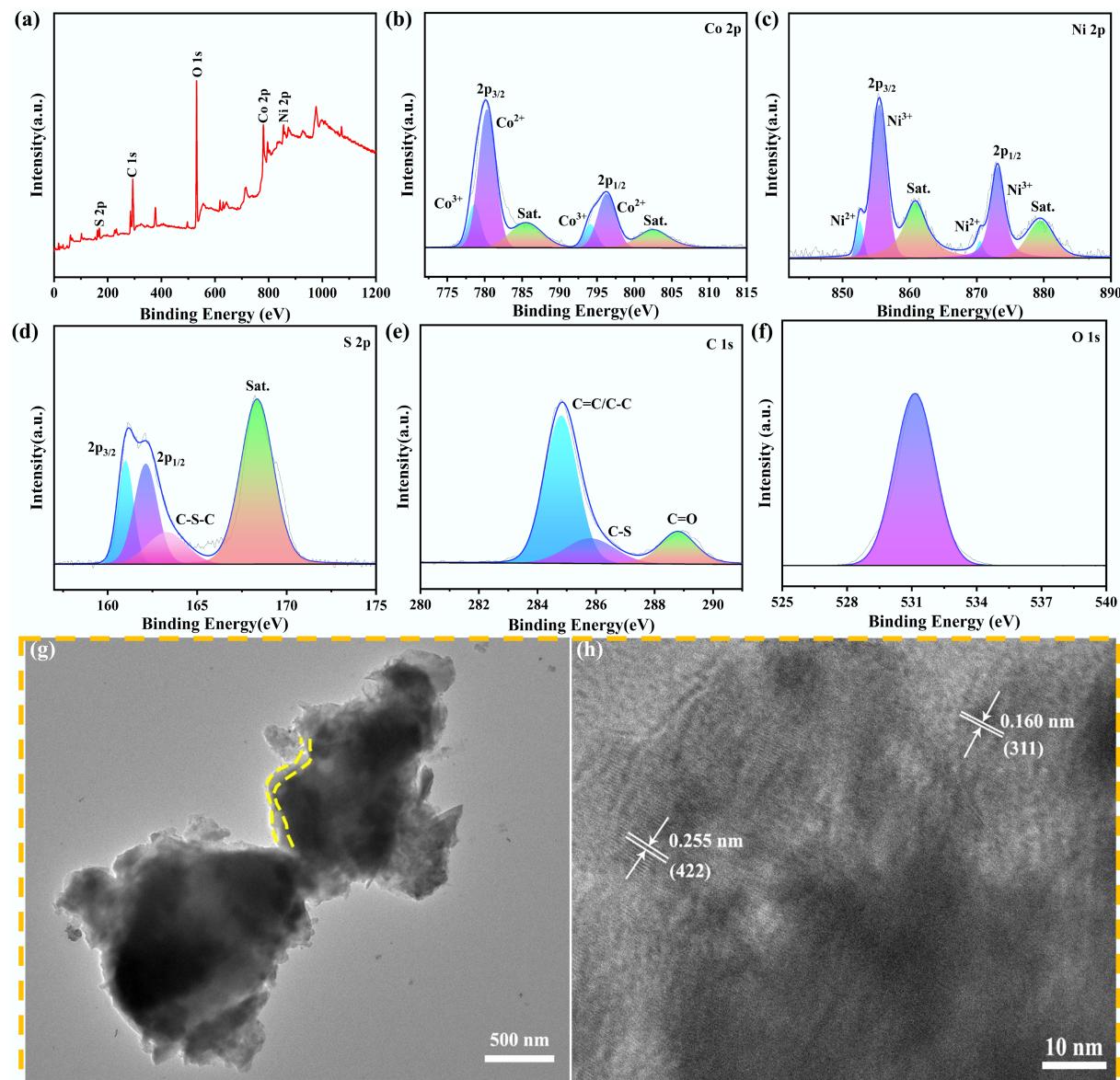
phenomenon further confirmed that NCS and all the NCS/CS@LC samples possessed a mesoporous structure. The BJH model was employed to calculate the pore size distribution based on the Kelvin equation, considering the effects of capillary condensation on adsorption capacity. The results are displayed in the corresponding insets of Fig. 1e, g, and Supplementary Fig. S1. Additionally, the BET specific surface area and BJH pore size data are compiled in Table 1. It was evident that as the lignin weight ratio increased, the specific surface area initially decreased and subsequently increased, whereas the pore size exhibited a gradual decreasing trend. This trend could be attributed to the fact that varying amounts of lignin induce distinct cross-linking and condensation reactions during the carbonization process, thereby leading to diverse morphologies and pore structures in the resulting products. It is well established that an appropriate specific surface area can offer a greater number of active sites, facilitating the insertion and expulsion of Na<sup>+</sup>. An optimal pore structure facilitates electrolyte infiltration and ion mobility, leading to enhanced cycling durability and rate capability in SIBs. When both the specific surface area and pore dimensions are small, the availability of active sites for Na<sup>+</sup>-involved electrochemical reactions decreases, hindering Na<sup>+</sup> migration and ultimately compromising the overall battery performance<sup>[19]</sup>. Conversely, if these parameters are excessively large, it may result in an increased occurrence of side reactions, which could significantly hinder the enhancement of electrochemical performance<sup>[20]</sup>. Subsequent studies demonstrated that NCS/CS@LC<sub>50</sub> exhibited superior cycling and rate performance due to its optimal balance between specific surface and pore size. The morphology of the synthesized material is illustrated in Fig. 1d, f, and Supplementary Fig. S2. Pure NiCo<sub>2</sub>S<sub>4</sub>,

which had not been co-carbonized with lignin, retained a spherical morphology, as previously reported<sup>[11]</sup>. Upon mixing NiCo<sub>2</sub>S<sub>4</sub> and lignin in an ethanol-water solution at varying weight ratios and subjecting the mixture to drying and calcination, significant morphological changes occurred, resulting in the formation of a new phase denoted as Co<sub>9</sub>S<sub>8</sub>. The composite phase NiCo<sub>2</sub>S<sub>4</sub>/Co<sub>9</sub>S<sub>8</sub> that formed was subsequently coated with carbon derived from lignin. It is evident that the weight ratio of lignin to NiCo<sub>2</sub>S<sub>4</sub> exerts a substantial impact on the morphology. When the lignin content is insufficient, phase separation or structural reorganization may occur at the interface between NiCo<sub>2</sub>S<sub>4</sub> and lignin during carbonization, leading to the agglomeration and stacking of product particles<sup>[21]</sup>, as depicted in Supplementary Fig. S2a. Upon increasing the dosage of lignin, the carbonized lignin forms a continuous carbon skeleton structure and efficiently encapsulates the spherical metal sulfides, thereby exhibiting a honeycomb-like morphology as depicted in Fig. 1f. When an excessive amount of lignin is introduced, during the carbonization process, a series of complex chemical reactions, including pyrolysis, polycondensation, and catalytic cracking, may intensify between NiCo<sub>2</sub>S<sub>4</sub> and lignin. These reactions significantly increase the specific surface area and result in structural collapse<sup>[22]</sup>, as illustrated in Supplementary Fig. S2b. Consequently, to achieve a honeycomb-like structure, it was optimal to utilize lignin at a weight ratio of 50%.

The surface elemental composition of the NCS/CS@LC<sub>50</sub> composite was comprehensively analyzed using XPS. As illustrated in Fig. 2a, the presence of elements such as Ni, Co, S, and C was confirmed. In Fig. 2b, the Co 2p spectrum exhibited spin-orbit splitting, typically manifested as two primary peaks at 780.11 and

**Table 1** The specific surface area, pore size, Warburg impedance factor ( $\sigma$ ) and  $\text{Na}^+$  diffusion coefficient of the as-synthesized samples

Sample	Specific surface area ( $\text{cm}^2 \text{ g}^{-1}$ )	Pore size (nm)	Warburg impedance factor ( $\sigma$ )	$\text{Na}^+$ diffusion coefficient $D$ ( $\text{cm}^2 \text{ s}^{-1}$ )	ICE (%)
NCS	15.11	23.68	300.30	$3.9 \times 10^{-12}$	53.15
NCS/CS@LC <sub>25</sub>	6.03	23.54	82.90	$5.1 \times 10^{-11}$	54
NCS/CS@LC <sub>50</sub>	42.25	12.98	36.21	$2.7 \times 10^{-10}$	65.61
NCS/CS@LC <sub>75</sub>	95.20	10.02	133.50	$2.0 \times 10^{-11}$	46.77

**Fig. 2** (a) XPS full spectrum and high-resolution XPS spectra of: (b) Co 2p, (c) Ni 2p, (d) S 2p, (e) C 1s, and (f) O 1s. (g) TEM image of NCS/CS@LC<sub>50</sub>. (h) Lattice fringes of NCS/CS@LC<sub>50</sub>.

796.22 eV, corresponding to Co 2p<sub>3/2</sub> and Co 2p<sub>1/2</sub>, respectively. In addition to the primary peaks, satellite peaks (designated as Sat.), located at 785.50 and 802.50 eV, were also observed. By employing peak fitting techniques, the experimental data were deconvoluted into multiple independent peaks; specifically, those observed at 780.30 and 796.30 eV were attributed to Co<sup>2+</sup> ions, while those detected at 778.60 and 794.10 eV corresponded to Co<sup>3+</sup> ions, indicating that both oxidation states were present in this sample<sup>[23]</sup>. The XPS spectra of the Ni 2p orbitals exhibited two prominent peaks

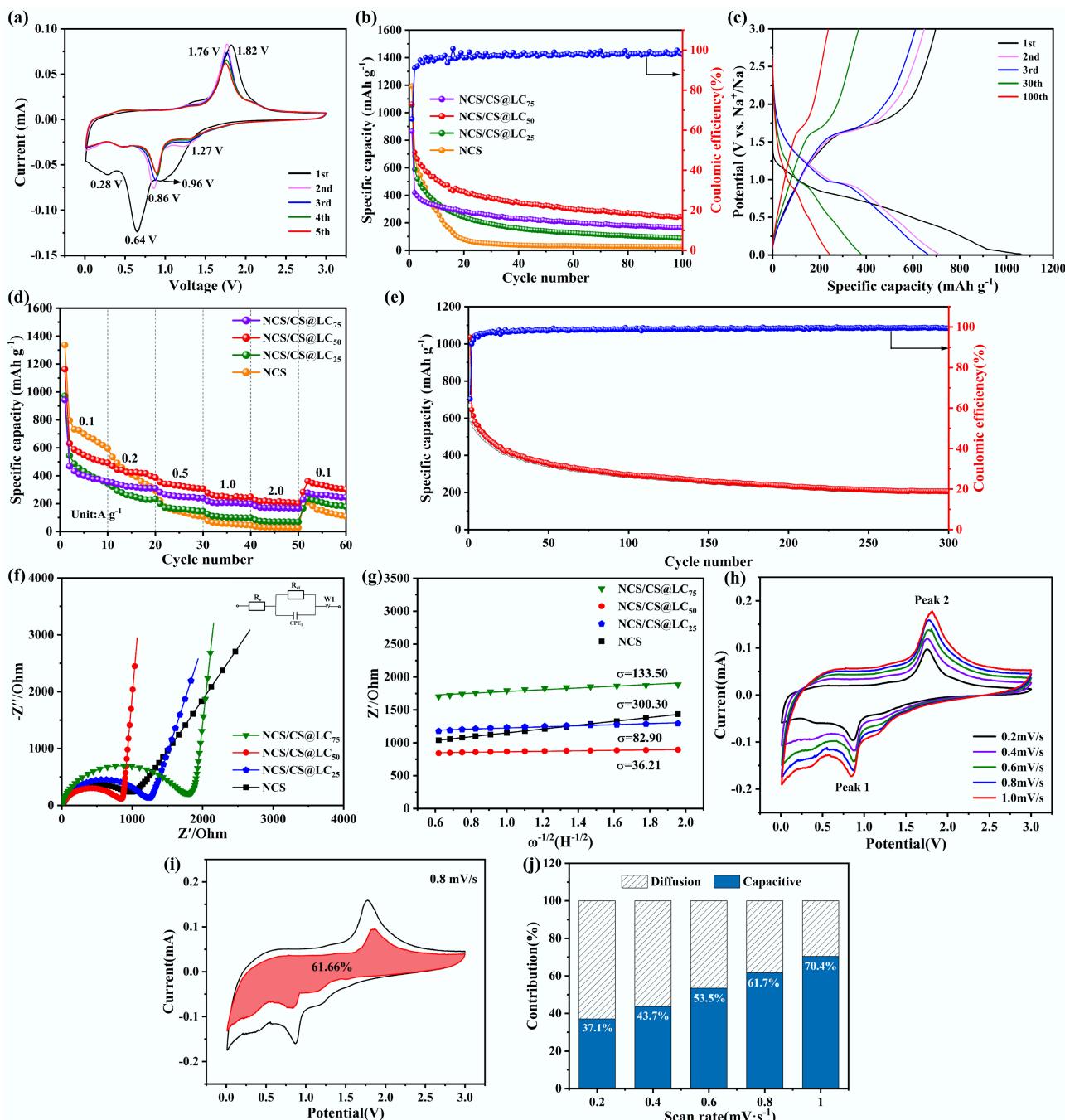
corresponding to 2p<sub>3/2</sub> and 2p<sub>1/2</sub>, along with their respective satellite peaks observed at 860.85 and 879.50 eV, as displayed in Fig. 2c. The binding energy of the 2p<sub>3/2</sub> peak was lower than that of the 2p<sub>1/2</sub> peak, and its intensity was comparatively higher. Similarly, upon fitting these splits within the Ni 2p orbital, two additional peaks were identified at energies of 852.55 and 870.49 eV, which were associated with Ni<sup>2+</sup>. Conversely, two more distinct peaks were found at 855.45 and 873.10 eV, attributable to Ni<sup>3+</sup>, thus confirming that Ni exists in the +2 and +3 oxidation states within this sample<sup>[24]</sup>.

The S 2p peak exhibited a spin-orbit splitting, resulting in two distinct sub-peaks, S 2p<sub>3/2</sub> and S 2p<sub>1/2</sub>, located at binding energies of 160.99 and 162.13 eV, respectively. The excitation effect, commonly observed in metal sulfides, resulted in the formation of satellite peaks situated at 168.35 eV, as illustrated in Fig. 2d. The peak situated at 163.29 eV, which was assigned to the C–S–C bond, corroborated the formation of carbon derived from lignin and its binding to metal sulfides. In the C 1s spectrum (Fig. 2e), the peaks at 284.81, 285.80, and 288.80 eV corresponded to the C=C/C–C, C–S, and C=O bonds, respectively. Finally, the peak at 531.14 eV, exhibited in the O 1s spectrum (Fig. 2f), may have resulted from the oxidation of the carbon layer surface or the incorporation of oxygen during the preparation of the composite. Figure 2g presents the TEM image of NCS/CS@LC<sub>50</sub>, which is in good agreement with its SEM image, once again indicating its honeycomb-like morphology. Furthermore, the presence of carbon layers in NCS/CS@LC<sub>50</sub> is illustrated in Fig. 2g, with some highlighted by yellow dotted lines. Figure 2h reveals the distinct lattice fringes of NCS/CS@LC<sub>50</sub>, further confirming its excellent crystallinity. Moreover, the plane spacings observed at 0.255 nm for NiCo<sub>2</sub>S<sub>4</sub> (422) and at 0.160 nm for Co<sub>9</sub>S<sub>8</sub> (311), as shown in Fig. 2h, illustrated the successful integration of NiCo<sub>2</sub>S<sub>4</sub> and Co<sub>9</sub>S<sub>8</sub> within the NCS/CS@LC<sub>50</sub> sample.

The synthesized material was coated onto a current collector copper foil, subsequently stamped, and assembled with sodium sheets to construct a sodium-ion half-cell for evaluating its electrochemical characteristics. Initially, the assembled sodium-ion half-cell underwent CV testing within a potential window of 0.01–3 V at a scan rate of 0.01 mV s<sup>-1</sup>. Figure 3a illustrates the CV curves for the initial five cycles of NCS/CS@LC<sub>50</sub>, while the CV plots for the other samples are provided in Supplementary Fig. S3. The CV curve revealed distinct oxidation and reduction peaks, indicating that NCS/CS@LC<sub>50</sub> exhibited favorable electrochemical activity in SIBs. In the initial CV curve, the reduction peak at 0.96 V corresponded to the insertion of Na<sup>+</sup> into NCS/CS@LC<sub>50</sub>, while reduction peaks at 0.64 and 0.28 V were associated with the reduction and deposition of electrolyte components on the surface of the negative electrode, leading to the formation of solid-electrolyte interphase (SEI) films, as well as the reduction of Co<sup>2+</sup>/Co<sup>3+</sup> and Ni<sup>2+</sup>/Ni<sup>3+</sup> to Co and Ni, respectively<sup>[25,26]</sup>. Correspondingly, the oxidation peak at 1.82 V was associated with the oxidation of Co and Ni to form CoS<sub>x</sub> and NiS<sub>x</sub>. In the subsequent CV plots, the reduction and oxidation peaks detected at 1.27, 0.86, and 1.76 V, respectively, correspond to the reduction and oxidation processes of Co<sup>2+</sup>/Co<sup>3+</sup> and Ni<sup>2+</sup>/Ni<sup>3+</sup>. From the second cycle onward, the CV curves largely overlapped, indicating that NCS/CS@LC<sub>50</sub> exhibited good reversibility<sup>[27]</sup>. Specifically, the insertion and extraction of Na<sup>+</sup> in the electrode material were reversible, with no significant changes in electrode structure or loss of active sites. Moreover, it was observed that the integral area of the CV curve during the first cycle was greater than that of subsequent cycles, indicating that the initial cycle of the electrode experienced a substantial amount of charge transfer during charging and discharging, thereby reflecting a higher specific capacity compared to later cycles. This phenomenon was further corroborated by the galvanostatic charge-discharge profile presented in Fig. 3b, c. The discharge capacity of NCS/CS@LC<sub>50</sub> was 1,062.8 mAh g<sup>-1</sup> during the first cycle, which gradually decreased as cycling progressed. The other samples exhibited analogous variation trends, as illustrated in Supplementary Fig. S4. The underlying reasons for this decline were as follows. The active material on the surface of NCS/CS@LC<sub>50</sub> may have reacted with the electrolyte to form an SEI layer, a process that consumed some of the active material<sup>[28]</sup>. As the charge-discharge cycles continued, the ongoing formation and reconfiguration of the

SEI layer may have further depleted the active material, leading to a gradual decline in specific capacity. In contrast, the initial Coulombic efficiency of NCS/CS@LC<sub>50</sub> was found to be superior to that of pure NCS, which is attributed to the incorporation of lignin-derived carbon layer. This carbon layer exhibits multiple synergistic effects, such as minimizing the irreversible consumption of SEI, mitigating the adsorption at defect sites, optimizing the arrangement of sodium storage active sites, enhancing conductivity, and strengthening the stability of the electrode-electrolyte interface<sup>[29]</sup>. Consequently, these effects collectively contributed to an enhancement in the initial Coulombic efficiency of NCS/CS@LC<sub>50</sub>. After 100 cycles, the specific capacities of NCS, NCS/CS@LC<sub>25</sub>, NCS/CS@LC<sub>50</sub>, and NCS/CS@LC<sub>75</sub> were measured at 27.2, 87.5, 244.5, and 162.7 mAh g<sup>-1</sup>, respectively, as illustrated in Fig. 3b. The maximum specific capacity exhibited by NCS/CS@LC<sub>50</sub> indicates that its specific surface area and pore dimensions have been precisely optimized, leading to improved electrical conductivity and structural stability as well as a reduced likelihood of side reactions. The initial Coulombic efficiency (ICE) serves as a key metric for assessing electrode reversibility and energy utilization efficiency. The calculated initial efficiencies of the synthesized samples are summarized in Table 1. Furthermore, as illustrated in Fig. 3c, the Coulombic efficiency of NCS/CS@LC<sub>50</sub> increased rapidly after the initial cycle for two primary reasons. This calculation result indicates that an appropriate carbon coating thickness can maximize the ICE by synergistically optimizing ion and electron transport, suppressing side reactions, and mitigating volume expansion. However, a coating that is either too thin or too thick will lead to reduced ICE. First, NCS/CS@LC<sub>50</sub> may demonstrate good structural stability during charging and discharging, which helps to minimize the shedding of active materials and the decomposition of the electrolyte, thereby enhancing Coulombic efficiency<sup>[30]</sup>. Second, as the charge-discharge cycles progressed, the SEI membrane gradually stabilized, reducing electrolyte consumption and active material loss. Consequently, the Coulombic efficiency experienced a rapid increase from the second cycle onward.

Figure 3d illustrates the rate performance of NCS/CS@LC<sub>50</sub>, which outperformed all other samples. At current densities of 0.1, 0.2, 0.5, 1, and 2 A g<sup>-1</sup>, the average discharge specific capacities were measured at 548.2, 423.3, 328.1, 247.1, and 208.7 mAh g<sup>-1</sup>, respectively. Upon decreasing the current density to 0.1 A g<sup>-1</sup>, the specific capacity was restored to 332.2 mAh g<sup>-1</sup>, rather than the initial 548.2 mAh g<sup>-1</sup>. The irreversible capacity loss may be attributed to lattice stress in electrode materials under high-rate operation, intensified interfacial side reactions, increased polarization, and the shedding or dissolution of active materials. Under high current charge and discharge conditions, the transport of Na<sup>+</sup> and electrons within the anode material may have been constrained, leading to some active substances being unable to participate in electrochemical reactions promptly<sup>[31]</sup>. Additionally, the anode material may have undergone significant volume changes or structural stresses. Moreover, it is essential for the anode material to possess rapid kinetic response capabilities to facilitate swift electrochemical reactions<sup>[32]</sup>. Consequently, as the current increased, the specific capacity tended to decrease. When the current was reduced, a rapid kinetic response from the anode material allowed for the recovery of specific capacity. This observation indicated that NCS/CS@LC<sub>50</sub> had effective ion and electron transport pathways capable of supporting rapid electrochemical reactions. NCS/CS@LC<sub>50</sub> could also maintain good structural stability after undergoing high-current charging and discharging cycles without severe structural damage or performance degradation. Furthermore, NCS/CS@LC<sub>50</sub> demonstrated commendable kinetic properties and stable electrochemical activity



**Fig. 3** (a) CV plot of first five cycles for NCS/CS@LC<sub>50</sub>. (b) Constant current charge-discharge profile of NCS/CS@LC<sub>50</sub> at a current of 0.1 A g<sup>-1</sup>. (c) Capacity-voltage curve of NCS/CS@LC<sub>50</sub> for 1<sup>st</sup>, 2<sup>nd</sup>, 3<sup>rd</sup>, 30<sup>th</sup>, and 100<sup>th</sup>. (d) Rate performance plot of NCS/CS@LC<sub>50</sub> at various current densities (0.1, 0.2, 0.5, 1.0, 2.0, and 0.1 A g<sup>-1</sup>). (e) Cycling performance of NCS/CS@LC<sub>50</sub> at a current density of 0.5 A g<sup>-1</sup>. (f) Nyquist diagram of synthesized NCS and NCS/CS@LC, accompanied by an equivalent circuit diagram as its illustration. (g) Straight line fitted between Z' and  $\omega^{-1/2}(H^{-1/2})$  at low frequencies for synthesized NCS and NCS/CS@LC. (h) CV measurements of NCS/CS@LC<sub>50</sub> electrode conducted at varying scan rates. (i) Pseudocapacitive contribution of NCS/CS@LC<sub>50</sub> electrode evaluated at a scan rate of 0.8 mV s<sup>-1</sup>. (j) Ratio of pseudocapacitance to diffusion control for NCS/CS@LC<sub>50</sub> electrode at varying sweep rates.

across varying current conditions. Overall, the aforementioned phenomena and analysis indicated that NCS/CS@LC<sub>50</sub> exhibited favorable ion and electron transport properties, exceptional structural stability, and promising kinetic characteristics. The long-term cycling performance of anode materials for sodium-ion batteries is a key indicator for assessing their practical applicability for Fig. 3e. It fundamentally reflects the material's ability to withstand structural degradation, accumulation of side reactions, and interfacial

deterioration during repeated Na<sup>+</sup> intercalation and deintercalation processes. As shown in Fig. 3e, NCS/CS@LC<sub>50</sub> exhibited stable cycling performance, retaining a specific capacity of 207 mAh g<sup>-1</sup> after 300 cycles at a current density of 0.5 A g<sup>-1</sup>, which demonstrates its excellent cycle stability. This favorable performance is attributed to the optimal thickness of the lignin-derived carbon coating, which effectively mitigates volume stress and suppresses metal ion dissolution. Furthermore, the SEM image of NCS/CS@LC<sub>50</sub>

after 300 cycles revealed that its hollow mesoporous structure remained well-preserved, further confirming its excellent cycling stability ([Supplementary Fig. S5](#)).

AC impedance analysis is frequently utilized to elucidate the internal impedance characteristics of batteries and assess the reaction kinetics of the electrodes, playing a crucial role in battery research. AC impedance measurements were performed using an electrochemical workstation across a frequency range of 100 kHz to 0.01 Hz at ambient temperature, resulting in the acquisition of Nyquist plots ([Fig. 3f](#)). Each Nyquist plot exhibited a semicircle in the high-frequency range and a straight line in the low-frequency range. The semicircle in the high-frequency range primarily represented the charge transfer impedance ( $R_{ct}$ ) at the electrode/electrolyte interface. During battery charging and discharging, charge must be transferred between the electrodes and the electrolyte, with the impedance of this process reflected in the high-frequency range<sup>[33]</sup>. The low-frequency range primarily reflected the diffusion process of ions within solid materials. In battery systems, ions must diffuse through solid electrode materials to participate in electrochemical reactions. The impedance associated with this process, referred to as Warburg impedance ( $Z_w$ ), is typically manifested in the low-frequency range as a diagonal line<sup>[34]</sup>. Furthermore, the intercept of the  $Z'$ -axis in the high-frequency range is regarded as the electrolyte impedance ( $R_e$ )<sup>[35]</sup>. The EIS spectra were meticulously analyzed using an equivalent circuit model with the aid of Zview software. The  $R_{ct}$  values of NCS, NCS/CS@LC<sub>25</sub>, NCS/CS@LC<sub>50</sub>, and NCS/CS@LC<sub>75</sub> were 855.3, 1,144.0, 790.3, and 1,651.0  $\Omega$ , respectively. The results indicated that the  $R_{ct}$  of NCS/CS@LC<sub>50</sub> was the lowest, attributable to three key factors. First, the regular and uniform honeycomb-like structure of NCS/CS@LC<sub>50</sub> facilitated a shorter diffusion path for ions, thereby reducing the  $R_{ct}$ . Second, the synergistic interaction between NiCo<sub>2</sub>S<sub>4</sub> and Co<sub>9</sub>S<sub>8</sub> may also have contributed to lowering the  $R_{ct}$  and enhancing its electrochemical performance. Third, the formation of lignin-derived carbon increased the conductivity of the material, which accelerated interfacial charge transfer and further diminished the  $R_{ct}$ <sup>[36]</sup>. This minimized energy loss during the transmission process, thereby allowing the SIBs to demonstrate superior electrochemical performance during both charging and discharging. Building upon this, the EIS data were utilized along with Eqs (1) and (2) to calculate the Na<sup>+</sup> diffusion coefficient ( $D$ )<sup>[37]</sup>. Initially, the Warburg coefficient ( $\sigma$ ) was determined through linear fitting of  $Z'$  and  $\omega^{-1/2}$ , as illustrated in [Fig. 3g](#). Subsequently,  $D$  was computed using Eq. (1), and the results are presented in [Table 1](#). As anticipated, the  $D$  of NCS/CS@LC<sub>50</sub> was found to be highest, indicating that Na<sup>+</sup> could be embedded into and detached from NCS/CS@LC<sub>50</sub> most rapidly, thereby further validating the optimal rate performance and minimal charge transfer resistance of NCS/CS@LC<sub>50</sub>.

$$D = R^2 T^2 / 2 A^2 n^4 F^4 C^2 \sigma^2 \quad (1)$$

$$Z' = R_e + R_{ct} + \sigma \omega^{-1/2} \quad (2)$$

To thoroughly assess the pseudocapacitive characteristics of NCS/CS@LC<sub>50</sub> and quantify the contribution of pseudocapacitance, CV measurements were performed at various scan rates of 0.2, 0.4, 0.6, 0.8, and 1 mV s<sup>-1</sup>, with results presented in [Fig. 3h](#). It was clear that as the sweep rate increased, the peak current also rose correspondingly. According to the Randles-Sevcik equation, there exists a linear correlation between the square root of the peak current and the sweep velocity, which accounts for this observed phenomenon. Furthermore, as the scan rate increased, both the oxidation and reduction peak potentials exhibited shifts; specifically, the oxidation peak shifted towards more positive potentials while the reduction

peak moved towards more negative potentials. This phenomenon was attributed to the fact that, for oxidation reactions, the concentration of electrons at the electrode surface decreases with increasing scan rate, as electrons are transferred more rapidly to the solution. To sustain the reaction, a higher electric potential is necessary to facilitate electron transfer; consequently, the oxidation peak potential shifts towards more positive values<sup>[16]</sup>. Conversely, in reduction reactions, the concentration of electrons at the electrode surface increases with rising scanning rates because electrons are transferred from the solution to the electrode more swiftly. In this scenario, a lower potential suffices to drive electron transfer, resulting in a shift of the reduction peak potential towards more negative values<sup>[38]</sup>.

Additionally, the  $b$ -value was utilized to identify the charge storage mechanism of NCS/CS@LC<sub>50</sub> throughout its charge and discharge cycles. First, the relationship between peak current ( $i$ ) and sweep velocity ( $v$ ), expressed as  $i = av^b$ , was transformed into a logarithmic form:  $\log(i) = b \times \log(v) + \log(a)$ . Subsequently, by performing a linear fit on  $\log(i)$  and  $\log(v)$ , the value of  $b$  was determined and is presented in [Supplementary Fig. S6](#); this was because  $b$  represented the slope of the fitted line. It is well-known that a  $b$ -value of 0.5 indicates battery-like behavior in the electrode material, with the corresponding process being governed by diffusion control. If the  $b$ -value is between 0.5 and 1, the electrode material displays characteristics of both battery and pseudocapacitance properties. When the  $b$ -value exceeds 1, it signifies that the electrode material primarily demonstrates pseudocapacitive behavior<sup>[39]</sup>. [Supplementary Fig. S6](#) clearly shows that the  $b$ -value was 0.65 for the reduction peak and 0.58 for the oxidation peak. This indicated that charge storage and release occurred through both ion diffusion within NCS/CS@LC<sub>50</sub> (cell behavior) and Faradaic processes at or within the electrode surface (pseudocapacitance behavior). These mechanisms contribute to enhancing the energy density, power density, and cycling stability of SIBs.

Furthermore, the pseudocapacitance contribution ratio was calculated. For each specific voltage value,  $k_1$  and  $k_2$  values were obtained by fitting  $i/v^{1/2}$  and  $v^{1/2}$  at different sweep rates using Eq. (4), which is mathematically derived from Eq. (3)<sup>[40]</sup>:

$$i = k_1 v + k_2 v^{1/2} \quad (3)$$

$$i/v^{1/2} = k_1 v^{1/2} + k_2 \quad (4)$$

where,  $i$  stands for current,  $v$  represents scan rate, and  $k_1$  and  $k_2$  are the fitting parameters.

Based on the  $k_1$  value obtained through fitting and the specific voltage value, as well as the sweep rate  $v$ , the current value contributed by the pseudocapacitor was calculated from  $i_{cap} = k_1 v$ . Then, using the voltage as the abscissa and the  $i_{cap}$  as the ordinate, the curve of the pseudocapacitance was plotted. Next, area fitting of the pseudocapacitance curve was performed to determine its contribution rate. The fitted pseudocapacitance curve was then compared with the original CV curve, allowing us to analyze the contribution of pseudocapacitive behavior to the total current<sup>[41]</sup>. The results are presented in [Fig. 3i, j](#). As illustrated in [Fig. 3i](#), pseudocapacitive behavior accounted for 61.66% of the total current at a sweep speed of 0.8 mV s<sup>-1</sup>. Additionally, it was evident from [Fig. 3j](#) that the contribution rate of pseudocapacitance increased with higher sweep rates. A high contribution rate enabled charge to be rapidly stored and released on or near the surface area of NCS/CS@LC<sub>50</sub>, enhancing both charge-discharge rates and energy output for the battery while improving cycle stability<sup>[42]</sup>; this allowed Na<sup>+</sup> to embed and detach more rapidly, thereby boosting the battery's rate performance.

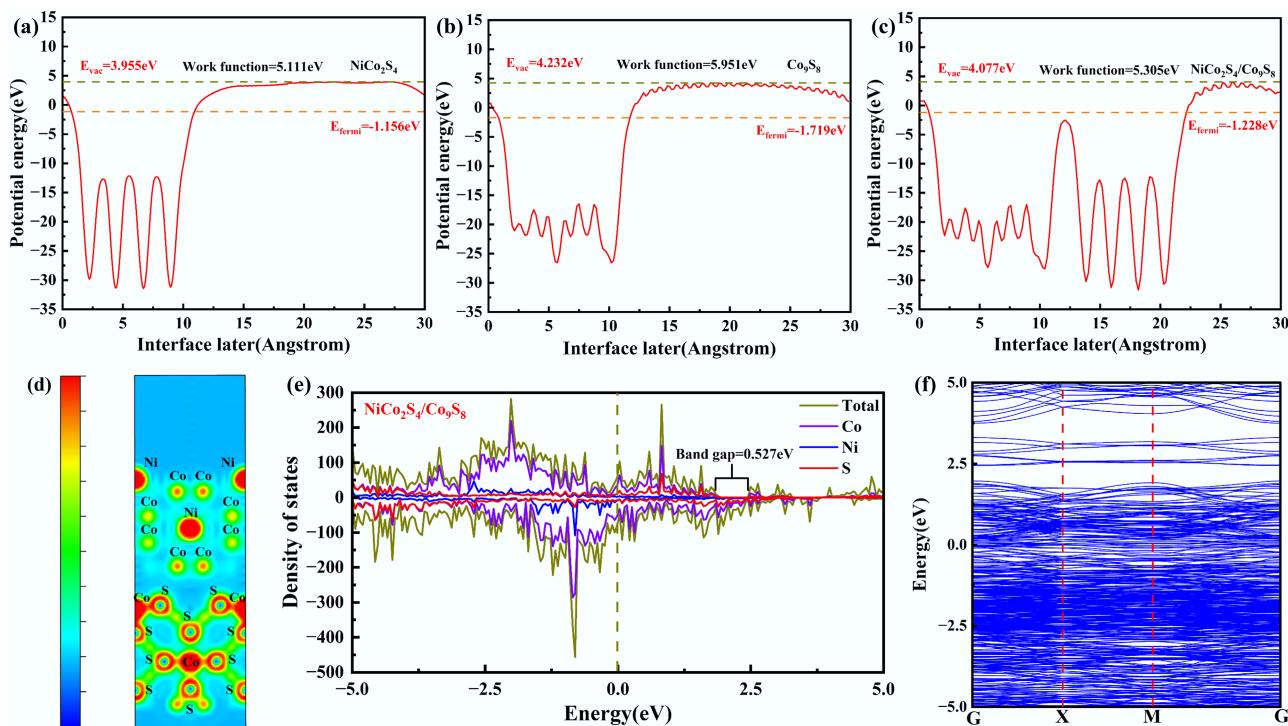
To elucidate the impact of the newly formed  $\text{Co}_9\text{S}_8$  phase on the electrochemical performance of  $\text{NiCo}_2\text{S}_4$  at the microstructural level, systematic calculations and analyses of electronic interactions at the  $\text{NiCo}_2\text{S}_4/\text{Co}_9\text{S}_8$  interface were conducted using density functional theory (DFT). As illustrated in Fig. 4a and b, the Fermi level of  $\text{NiCo}_2\text{S}_4$  was calculated to be  $-1.156$  eV, which was marginally higher than that of  $\text{Co}_9\text{S}_8$  ( $-1.719$  eV). This subtle difference in energy levels exerts a notable influence when the two materials form a heterojunction<sup>[43]</sup>. Once the generated  $\text{Co}_9\text{S}_8$  is coated onto  $\text{NiCo}_2\text{S}_4$ , a contact potential difference forms at the interface, facilitating electron transfer from the inner  $\text{NiCo}_2\text{S}_4$  to the outer  $\text{Co}_9\text{S}_8$ . From the standpoint of electronic work function analysis, the  $\text{NiCo}_2\text{S}_4/\text{Co}_9\text{S}_8$  heterostructure exhibited a work function of  $5.305$  eV (as depicted in Fig. 4c), which was intermediate between those of pure  $\text{NiCo}_2\text{S}_4$  ( $5.111$  eV) and pure  $\text{Co}_9\text{S}_8$  ( $5.951$  eV). This observation suggests that the electromotive force of  $\text{NiCo}_2\text{S}_4/\text{Co}_9\text{S}_8$  is predominantly governed by  $\text{Co}_9\text{S}_8$ , highlighting the critical influence of  $\text{Co}_9\text{S}_8$  in determining the overall electrochemical performance of  $\text{NiCo}_2\text{S}_4/\text{Co}_9\text{S}_8$ <sup>[43]</sup>. Figure 4d presents the charge density difference for the interface of  $\text{NiCo}_2\text{S}_4/\text{Co}_9\text{S}_8$ , showing that sulfur atoms located in the shell layer donate electrons, whereas cobalt atoms supply holes, thereby establishing a charge transfer pathway. Furthermore, these shell-layer sulfur atoms engage in additional charge transfer pathways with both nickel and cobalt atoms situated in the core layer. The density of states (DOS) and band structure of  $\text{NiCo}_2\text{S}_4/\text{Co}_9\text{S}_8$  were computed to obtain a more comprehensive understanding of its intrinsic electronic properties. The band structure presented in Fig. 4f aligns well with the corresponding DOS profile (Fig. 4e), as regions exhibiting pronounced DOS peaks correspond to densely populated segments of the band structure<sup>[44]</sup>. The electronic states near the Fermi level predominantly arise from Ni-3d, Co-2p, and S-2p orbitals. The elevated DOS near the Fermi level of  $\text{NiCo}_2\text{S}_4/\text{Co}_9\text{S}_8$  suggests that this composite exhibits superior

electrical conductivity<sup>[45]</sup>. Combined with the favorable conductive properties of lignin-derived carbon, this feature contributes to the enhanced sodium storage performance of  $\text{NiCo}_2\text{S}_4/\text{Co}_9\text{S}_8@\text{LC}$ . The bandgap configuration ( $0.527$  eV), as shown in Fig. 4e, is sufficiently wide to prevent the reduction of open-circuit voltage that typically arises from an excessively narrow bandgap. The relatively wide bandgap contributes to mitigating energy losses associated with non-radiative recombination during electrochemical processes, thereby enhancing the overall energy conversion efficiency<sup>[43]</sup>. Thus, DFT-based theoretical calculations reveal that  $\text{NiCo}_2\text{S}_4/\text{Co}_9\text{S}_8@\text{LC}$  possesses superior electronic transport properties and low charge transfer resistance, endowing it with significant potential as an anode material for SIBs.

Ultimately, the sodium storage performance of  $\text{NCS/CS}@\text{LC}_{50}$  synthesized from spent mobile phone batteries and modified with lignin-derived carbon was evaluated against previously reported data (Table 2). The results demonstrated that its electrochemical performance is comparable or slightly inferior to that of previously reported  $\text{NiCo}_2\text{S}_4$  prepared by analytic reagents. However, this study successfully achieved the high-value utilization of waste resources. The resulting material,  $\text{NCS/CS}@\text{LC}_{50}$ , exhibits excellent sodium storage performance while being derived from sustainable and environmentally benign feedstocks, demonstrating its significant potential for industrial application. This approach not only substantially reduces the manufacturing cost and enhances the market competitiveness of SIBs but also facilitates their large-scale deployment in smart grids, electric vehicles, and various electronic devices.

## Conclusions

In this research,  $\text{NCS/CS}@\text{LC}_{50}$  was prepared via a hydrothermal process utilizing spent mobile phone batteries and industrial lignin as the primary raw materials. The composite integrated the high



**Fig. 4** Calculated work function of (a)  $\text{NiCo}_2\text{S}_4$ , (b)  $\text{Co}_9\text{S}_8$ , and (c)  $\text{NiCo}_2\text{S}_4/\text{Co}_9\text{S}_8$ . (d) Charge density difference for the interface of  $\text{NiCo}_2\text{S}_4/\text{Co}_9\text{S}_8$ . (e) Density of state, and (f) band structure for  $\text{NiCo}_2\text{S}_4/\text{Co}_9\text{S}_8$ .

**Table 2** Comparison of the electrochemical performance of the synthesized NCS/CS@LC<sub>50</sub> in this study with that of NiCo<sub>2</sub>S<sub>4</sub> reported in the literature

Materials	Current density (A g <sup>-1</sup> )	Specific capacity (mAh g <sup>-1</sup> )/cycle number	Ref.
NiCo <sub>2</sub> S <sub>4</sub> @CNTs	0.05	291/80	[46]
NiCo <sub>2</sub> S <sub>4</sub> @CNF	2.0	283/400	[47]
NiCo <sub>2</sub> S <sub>4</sub> @Ni-B	1.0	252/200	[48]
NiCo <sub>2</sub> S <sub>4</sub> @MoS <sub>2</sub>	3.2	158/400	[49]
NCS@GNs@CNTs	0.2	363/100	[50]
NCSGO	1.0	250/350	[51]
NiCo <sub>2</sub> S <sub>4</sub> /Co <sub>9</sub> S <sub>8</sub> @LC <sub>50</sub>	1.0	245/100	This work

electrochemical activity of NiCo<sub>2</sub>S<sub>4</sub> and Co<sub>9</sub>S<sub>8</sub> with the excellent electrical conductivity of carbon materials, presenting unique structural and performance advantages. Electrochemical testing revealed that the NCS/CS@LC<sub>50</sub> demonstrated high reversible specific capacity, good cycling stability, and exceptional rate performance. These enhancements in performance were primarily attributed to the synergistic effects of its various components and the distinctive structure of this composite. Specifically, NiCo<sub>2</sub>S<sub>4</sub> and Co<sub>9</sub>S<sub>8</sub> provided a rich array of redox reaction sites, facilitating the Na<sup>+</sup> intercalation/deintercalation; additionally, the incorporation of carbon materials enhanced overall electrode conductivity, promoting rapid electron transport. Furthermore, this study considered the effect of lignin-derived carbon on the morphology of NCS/CS@LC, providing valuable references for further optimizing the performance of composite materials. Simultaneously, the feasibility of utilizing spent mobile phone batteries and industrial lignin as raw materials to prepare high-performance sodium storage materials was also validated, providing a new perspective on the resource utilization of spent batteries and industrial lignin.

## Supplementary information

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## Author contributions

The authors confirm their contributions to the paper as follows: Changwei Dun: conceptualization, investigation, methodology, formal analysis, writing – original draft, funding acquisition, resources, writing – review and editing; Yizhao Zhao: investigation, methodology, data curation; Pengpeng Zhang: conceptualization, investigation, formal analysis, data curation; Hua Lv: conceptualization, resources; Yumin Li: methodology, supervision; Yuebin Xi: funding acquisition, supervision, methodology, formal analysis, writing – review and editing; Xijun Zhang: resources, conceptualization, investigation; Rui Liang: conceptualization, supervision. All authors reviewed the results and approved the final version of the manuscript.

## Data availability

All data generated or analyzed during this study are included in this published article and its supplementary information files.

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## Declarations

### Competing interests

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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